

环形截面螺旋管道内的粘性流动

章本照

D. N. Fan

(浙江大学力学系, 310027) (美国 Howard 大学, DC., 20059)

提要 根据张量分析, 建立了非正交的曲线柱坐标系中的 N-S 方程. 采用摄动法求解环形截面螺旋管道内的粘性流动. 结果表明: 环形截面上存在二次流.

关键词 张量应用, 螺旋管道, 二次流, 摄动解

一、前 言

曲线管道中的粘性流动, 对于生物力学和流体工程的应用, 关系密切. 但是, 如在常用的坐标系中求解, 是十分困难的. 本文建立了曲线柱坐标系, 推导了这个坐标系中的 N-S 方程, 从而为研究一般曲线管道中的流动, 提供了方便的数学方程. 对曲线管道流动进行开创性工作的 Dean 所采用的圆环坐标^[1,2]以及 Y. C. Wang 所采用的螺旋坐标^[3]都是本文所建立的曲线柱坐标系的特例.

本文从曲线柱坐标系中的 N-S 方程出发, 采用摄动法求解了环形截面螺旋管道中的粘性流动. 和前人工作^[4]比较, 特点是: 螺旋管道是环形截面, 曲率和挠率可以是任意的, 但作了截面环形宽度相对内圆半径是小量的假定. 结果表明: 环形截面上出现二次流动.

二、曲线柱坐标系中的 Navier-Stokes 方程

假定给出任意空间曲线

$$\mathbf{R} = \mathbf{R}(s) = X(s)\mathbf{e}_x + Y(s)\mathbf{e}_y + Z(s)\mathbf{e}_z$$

其中 $\mathbf{e}_x, \mathbf{e}_y, \mathbf{e}_z$ 是某一给定的笛卡尔坐标系的基矢量; $X(s), Y(s), Z(s)$ 是已知的坐标函数; s 是曲线由某一起始点起算的曲线弧长. 显然, 曲线的曲率 κ 和挠率 τ 可由坐标函数计算获得. 曲线的切线, 法线和付法线的单位矢量分别为

$$\mathbf{T} = \frac{d\mathbf{R}}{ds}, \mathbf{N} = \frac{1}{\kappa} \frac{d\mathbf{T}}{ds}, \mathbf{B} = \mathbf{T} \times \mathbf{N}$$

它们是互为正交的.

我们不妨在 $\mathbf{N}, \mathbf{B}$ 所构成的平面中定义极坐标 (r, θ) , $\mathbf{N}$ 方向上 $\theta = 0$. 这样空间任

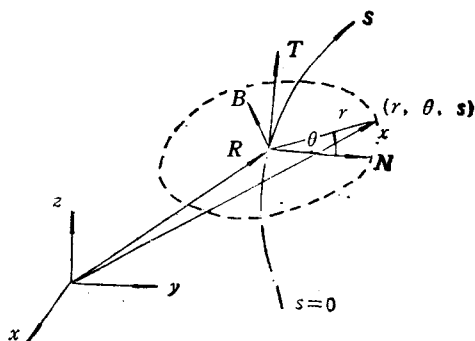


图 1 曲线柱坐标系

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一点的坐标矢量可以表示为

$$\mathbf{x} = \mathbf{R}(s) + r \cos \theta \mathbf{N}(s) + r \sin \theta \mathbf{B}(s)$$

于是可引进 (r, θ, s) 作为曲线坐标变量; 相应的坐标系称为曲线柱坐标系. 应当注意到这个坐标系的基矢量 $\mathbf{e}_r, \mathbf{e}_\theta, \mathbf{e}_s$ 是非正交的, 为此引进互为正交的物理基矢量 $(\mathbf{r}_0, \boldsymbol{\theta}_0, \mathbf{n}_0)$, 定义为

$$\mathbf{r}_0 = \mathbf{e}_r, \quad \boldsymbol{\theta}_0 = \mathbf{e}_\theta / |\mathbf{e}_\theta|, \quad \mathbf{n}_0 = \mathbf{T}$$

任一物理量 $\mathbf{A}$, 物理基上的逆变分量为 A^r, A^θ, A^s .

根据张量流体力学理论^[9], 经严格推导, 可获得曲线柱坐标系中的 Navier-Stokes 方程

$$\begin{aligned} & \frac{\partial v^r}{\partial t} + \frac{1}{r} \frac{\partial v^\theta}{\partial \theta} + \frac{\tau}{m} \frac{\partial v^s}{\partial \theta} + \frac{1}{m} \frac{\partial v^s}{\partial s} + \left(2 - \frac{1}{m}\right) \frac{v^r}{r} + \frac{m_\theta}{rm} v^\theta = 0 \\ & \frac{\partial v^r}{\partial t} + v^r \frac{\partial v^r}{\partial r} + \left(\frac{v^\theta}{r} - \frac{\tau v^s}{m}\right) \frac{\partial v^r}{\partial \theta} + \frac{v^s}{m} \frac{\partial v^r}{\partial s} - \frac{(v^\theta)^2}{r} - \frac{m_r (v^s)^2}{m} \\ & \quad - \frac{1}{\rho} \frac{\partial p}{\partial r} + v(\nabla^2 \mathbf{v})^r \\ & \frac{\partial v^\theta}{\partial t} + v^r \frac{\partial v^\theta}{\partial r} + \left(\frac{v^\theta}{r} - \frac{\tau v^s}{m}\right) \frac{\partial v^\theta}{\partial \theta} + \frac{v^s}{m} \frac{\partial v^\theta}{\partial s} - \frac{v^r v^\theta}{r} - \frac{m_\theta (v^s)^2}{rm} \\ & \quad - \frac{1}{\rho r} \frac{\partial p}{\partial \theta} + v(\nabla^2 \mathbf{v})^\theta \\ & \frac{\partial v^s}{\partial t} + v^r \frac{\partial v^s}{\partial r} + \left(\frac{v^\theta}{r} - \frac{\tau v^s}{m}\right) \frac{\partial v^s}{\partial \theta} + \frac{v^s}{m} \frac{\partial v^s}{\partial s} - \frac{m_r v^r v^s}{m} - \frac{m_\theta v^\theta v^s}{rm} \\ & \quad - \frac{1}{\rho m} \left(\frac{\partial p}{\partial s} - \tau \frac{\partial p}{\partial \theta} \right) + v(\nabla^2 \mathbf{v})^s \end{aligned} \quad (1)$$

其中

$$\begin{aligned} (\nabla^2 \mathbf{v})^r &= \frac{\partial^2 v^r}{\partial r^2} + \left(\frac{1}{r^2} + \frac{\tau^2}{m^2}\right) \frac{\partial^2 v^r}{\partial \theta^2} + \frac{1}{m^2} \frac{\partial^2 v^r}{\partial s^2} - \frac{2\tau}{m^2} \frac{\partial^2 v^r}{\partial \theta \partial s} + \left(\frac{1}{r} + \frac{m_r}{m}\right) \frac{\partial v^r}{\partial r} \\ &+ \left[\frac{m_\theta}{m} \left(\frac{1}{r^2} - \frac{\tau^2}{m^2}\right) + \frac{\tau m_s}{m^3} - \frac{\tau_s}{m^2}\right] \frac{\partial v^r}{\partial \theta} + \frac{1}{m^3} (\tau m_\theta - m_s) \frac{\partial v^r}{\partial s} \\ &- \frac{2}{r^2} \frac{\partial v^\theta}{\partial \theta} + \frac{2\tau m_r}{m^2} \frac{\partial v^\theta}{\partial \theta} - \frac{2m_r}{m^2} \frac{\partial v^\theta}{\partial s} - \left(\frac{1}{r^2} + \frac{m_r^2}{m^2}\right) v^r \\ &- \frac{m_\theta}{rm^2} \left(m_r + \frac{m}{r}\right) v^\theta + \frac{1}{m^2} \left(\tau m_{r\theta} - \frac{\tau}{m} m_r m_\theta - m_{rs} + \frac{1}{m^2} m_r m_s\right) v^s \\ (\nabla^2 \mathbf{v})^\theta &= \frac{\partial^2 v^\theta}{\partial r^2} + \left(\frac{1}{r^2} + \frac{\tau}{m^2}\right) \frac{\partial^2 v^\theta}{\partial \theta^2} + \frac{1}{m^2} \frac{\partial^2 v^\theta}{\partial s^2} - \frac{2\tau}{m^2} \frac{\partial^2 v^\theta}{\partial \theta \partial s} + \frac{2}{r^2} \frac{\partial v^r}{\partial \theta} \\ &+ \left(\frac{1}{r} + \frac{m_r}{m}\right) \frac{\partial v^\theta}{\partial r} + \left[\frac{1}{m} \left(\frac{1}{r^2} - \frac{\tau^2}{m^2}\right) m_\theta + \frac{1}{m^2} \left(\frac{\tau m_s}{m} - \tau_s\right)\right] \frac{\partial v^\theta}{\partial \theta} \\ &+ \frac{1}{m^3} (\tau m_\theta - m_s) \frac{\partial v^\theta}{\partial s} + \frac{2\tau m_\theta}{rm^2} \frac{\partial v^\theta}{\partial \theta} - \frac{2m_\theta}{rm^2} \frac{\partial v^\theta}{\partial s} + \frac{m_\theta}{rm^2} \left(\frac{m}{r} - m_r\right) v^r \\ &- \frac{1}{r^2} \left(1 + \frac{m_\theta^2}{m}\right) v^\theta + \frac{1}{rm^2} \left(\tau m_{\theta\theta} - \frac{\tau}{m} m_\theta^2 + \frac{1}{m} m_\theta m_s - m_{\theta s}\right) v^s \end{aligned}$$

$$\begin{aligned}
(\nabla^2 v)^n = & \frac{\partial^2 v^n}{\partial r^2} + \left(\frac{1}{r^2} + \frac{\tau^2}{m^2}\right) \frac{\partial^2 v^n}{\partial \theta^2} + \frac{1}{m^2} \frac{\partial^2 v^n}{\partial s^2} - \frac{2\tau}{m^2} \frac{\partial^2 v^n}{\partial \theta \partial s} - \frac{2\tau m_r}{m^2} \frac{\partial v^n}{\partial \theta} \\
& + \frac{2m_r}{m^2} \frac{\partial v^n}{\partial s} - \frac{2\tau m_\theta}{r m^2} \frac{\partial v^\theta}{\partial \theta} + \frac{2m_\theta}{r m^2} \frac{\partial v^\theta}{\partial s} + \left(\frac{1}{r} + \frac{m_r}{m}\right) \frac{\partial v^n}{\partial r} \\
& + \frac{1}{m^2} \left[\left(\frac{m}{r^2} - \frac{\tau^2}{m}\right) m_\theta + \frac{\tau m_s}{m} - \tau_s \right] \frac{\partial v^n}{\partial \theta} + \frac{1}{m^3} (\tau m_\theta - m_s) \frac{\partial v^n}{\partial s} \\
& + \frac{1}{m^2} \left(\frac{\tau}{m} m_r m_\theta - \tau m_{rs} + m_{rs} - \frac{1}{m} m_r m_s \right) v^n - \frac{1}{r m^3} \\
& \cdot (\tau m m_{\theta\theta} - \tau m_\theta^2 - m m_{\theta s} + m_\theta m_s) v^\theta - \frac{1}{m^2} \left(m_r^2 + \frac{m_\theta^2}{r^2} \right) v^n \quad (2)
\end{aligned}$$

上述式中

$$\begin{aligned}
m &= 1 - \kappa r \cos \theta, \quad m_r \equiv \frac{\partial m}{\partial r} = -\kappa \cos \theta, \quad m_\theta \equiv \frac{\partial m}{\partial \theta} = \kappa r \sin \theta \\
m_s &\equiv \frac{\partial m}{\partial s} = -r \cos \theta \frac{d\kappa}{ds}, \quad m_{r\theta} \equiv \frac{\partial^2 m}{\partial r \partial \theta} = \kappa \sin \theta, \quad m_{rs} \equiv \frac{\partial^2 m}{\partial r \partial s} = -\cos \theta \frac{d\kappa}{ds} \\
m_{\theta\theta} &\equiv \frac{\partial^2 m}{\partial \theta^2} = \kappa r \cos \theta, \quad m_{\theta s} \equiv \frac{\partial^2 m}{\partial \theta \partial s} = r \sin \theta \frac{d\kappa}{ds}, \quad \tau_s \equiv \frac{d\tau}{ds} \quad (3)
\end{aligned}$$

显然, 当 $\kappa = \text{const}$, $r = 0$ 时, 上述方程组即为文献 [4] 中的圆环坐标系中的方程形式。

同样, 还可推导出粘性应力张量各分量的表达式:

$$\begin{aligned}
T^{rr} &= 2\mu \frac{\partial v^r}{\partial r} \\
T^{r\theta} &= \mu \left[\left(\frac{1}{r^2} + \frac{\tau^2}{m^2}\right) \frac{\partial v^r}{\partial \theta} + \frac{1}{r} \frac{\partial v^\theta}{\partial r} - \frac{\tau}{m^2} \frac{\partial v^r}{\partial s} - \frac{\tau}{m} \frac{\partial v^n}{\partial r} - \frac{v^\theta}{r} + \frac{\tau m_r}{m^2} v^n \right] \\
T^{rs} &= \mu \left(\frac{1}{m} \frac{\partial v^n}{\partial r} + \frac{1}{m^2} \frac{\partial v^r}{\partial s} - \frac{\tau}{m^2} \frac{\partial v^r}{\partial \theta} - \frac{m_r}{m^2} v^n \right) \\
T^{\theta r} &= \mu \left(\frac{\partial v^\theta}{\partial r} + \frac{1}{r} \frac{\partial v^r}{\partial \theta} - \frac{v^\theta}{r} \right) \\
T^{\theta\theta} &= \mu \left[\left(\frac{2}{r^2} + \frac{\tau^2}{m^2}\right) \frac{\partial v^\theta}{\partial \theta} - \frac{\tau}{m^2} \frac{\partial v^\theta}{\partial s} - \frac{\tau}{r m} \frac{\partial v^n}{\partial \theta} + \frac{\tau m_\theta}{r m^2} v^n + \frac{2}{r^2} v^r \right] \\
T^{\theta s} &= \mu \left(\frac{1}{r m} \frac{\partial v^n}{\partial \theta} + \frac{1}{m^2} \frac{\partial v^\theta}{\partial s} - \frac{\tau}{m^2} \frac{\partial v^\theta}{\partial \theta} - \frac{m_\theta}{r m^2} v^n \right) \\
T^{sr} &= \mu \left(\frac{\partial v^n}{\partial r} - \frac{\tau}{m} \frac{\partial v^r}{\partial \theta} + \frac{1}{m} \frac{\partial v^r}{\partial s} - \frac{m_r}{m} v^n \right) \\
T^{s\theta} &= \mu \left[\left(\frac{1}{r^2} + 2 \frac{\tau^2}{m^2}\right) \frac{\partial v^n}{\partial \theta} + \frac{1}{r m} \frac{\partial v^\theta}{\partial s} - \frac{\tau}{r m} \frac{\partial v^\theta}{\partial \theta} - \frac{2\tau}{m^2} \frac{\partial v^n}{\partial s} \right. \\
&\quad \left. - \frac{2\tau m_r}{m^2} v^r - 2 \frac{\tau m_\theta}{r m^2} v^\theta - \frac{m_\theta}{r^2 m} v^n \right] \\
T^{nn} &= 2\mu \left(-\frac{\tau}{m^2} \frac{\partial v^n}{\partial \theta} + \frac{1}{m^2} \frac{\partial v^n}{\partial s} + \frac{m_r}{m^2} v^r + \frac{m_\theta}{r m^2} v^\theta \right)
\end{aligned}$$

以上各式中的 ρ, μ, ν 分别是流体的密度, 动力粘性系数和运动粘性系数。

三、环形截面螺旋管道中粘性流的摄动解

1. 问题的提出

考虑如图 2 所示的环形截面螺旋管道,管道中心线的曲率 κ 和挠率 τ 均为已知常数.

环形截面的内圆半径为 R ,外圆半径为 $(R + d)$.

在所考虑的问题中,假定:

- (1) 流动为不可压,定常,层流.
- (2) 螺旋管道充分长,忽略管道进口影响,即

$$\frac{\partial v^i}{\partial s} = 0 \quad (i = r, \theta, n)$$

- (3) d 相对 R 是小量, $d/R \equiv \varepsilon \ll 1$.
- (4) 粘性力与压力梯度同一量级.

根据上述第(3),(4)两点假定,通过方程可作出量级估计: $v^r \sim o(1)$, $v^\theta \sim o(1)$, $v^r \sim o(\varepsilon)$, $p \sim o(1/\varepsilon^2)$; 于是可将各物理量展成小参数 ε 的

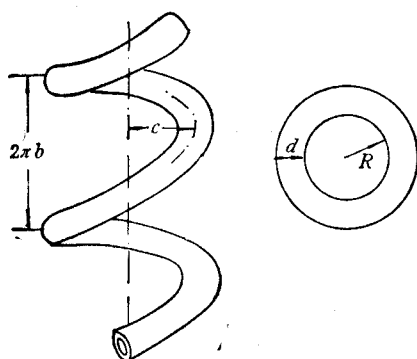


图 2 环形截面的螺旋管道

无量纲量的幂级数

$$\begin{aligned} v^r &= U(v_0^r + \varepsilon v_1^r + \varepsilon^2 v_2^r + \cdots) \\ v^\theta &= U(v_0^\theta + \varepsilon v_1^\theta + \varepsilon^2 v_2^\theta + \cdots) \\ v^r &= \varepsilon U(v_0^r + \varepsilon v_1^r + \varepsilon^2 v_2^r + \cdots) \\ p &= \frac{\rho U^2}{\varepsilon^2 \text{Re}} \{ [a_0 z + p_0(\eta, \theta)] + \varepsilon [a_1 z + p_1(\eta, \theta)] \\ &\quad + \varepsilon^2 [a_2 z + p_2(\eta, \theta)] + \cdots \} \end{aligned} \quad (4)$$

其中 $\text{Re} \equiv RU/\nu$; 无量纲坐标变量为

$$\eta = \frac{r-R}{d} = \frac{1}{\varepsilon} \left(\frac{r}{R} - 1 \right), \theta = \theta, z = \frac{s}{R} \quad (5)$$

特征量 U 是环形截面上的法向平均速度; 若记流量为 Q^* , 则有

$$Q^* = U\pi[(R+d)^2 - R^2] = U\pi R^2(2\varepsilon + \varepsilon^2)$$

不妨定义无量纲流量

$$Q \equiv Q^*/U\pi R^2 = 2\varepsilon + \varepsilon^2 \quad (6)$$

无量纲的曲率和挠率定义为

$$\kappa_0 = \kappa R \quad \tau_0 = \tau_0 R \quad (7)$$

2. 零阶摄动解

将(4),(5),(7)式代入(1),(2)式中,比较 ε 的量阶,且注意到 κ_0, τ_0 是常数, $\frac{\partial v^i}{\partial z} =$

0; 即可得到关于 ε 的零阶方程

$$\begin{aligned} \frac{\partial v_0^r}{\partial \eta} + \frac{\partial v_0^\theta}{\partial \theta} - \frac{\tau_0}{m_0} \frac{\partial v_0^\theta}{\partial \theta} + \frac{m_0'}{m_0} v_0^\theta &= 0 \\ \frac{\partial p_0}{\partial \eta} &= 0 \end{aligned}$$

$$\begin{aligned}\frac{\partial p_0}{\partial \theta} - \frac{\partial^2 v_0^\theta}{\partial \eta^2} &= 0 \\ \frac{1}{m_0} \left(a_0 - \tau_0 \frac{\partial p_0}{\partial \theta} \right) - \frac{\partial^2 v_0^n}{\partial \eta^2} &= 0\end{aligned}\quad (8)$$

上式中

$$m_0 \equiv 1 - \kappa_0 \cos \theta \quad m'_0 \equiv \frac{dm_0}{d\theta} = \kappa_0 \sin \theta \quad (9)$$

边界条件:

$$\text{在 } \eta = 0, \eta = 1 \text{ 上} \quad v_0^n = v_0^\theta = v'_0 = 0 \quad (10)$$

压力和速度还应满足周期性条件

$$p_0(\eta, 0) = p_0(\eta, 2\pi), \quad v'_0(\eta, 0) = v'_0(\eta, 2\pi) \quad (i = r, \theta, n) \quad (11)$$

利用边界条件(10)和周期性条件(11), 求解方程组(8)式, 经过复杂的积分运算, 可获得

$$\begin{aligned}v'_0 &= 0 \\ v_0^\theta &= -\frac{a_0}{2} \frac{\tau_0(1 - c_0 m_0)}{m'_0 + \tau_0^2} (\eta - \eta^2) \\ v_0^n &= -\frac{a_0}{2} \frac{m_0 + c_0 \tau_0^2}{m_0^2 + \tau_0^2} (\eta - \eta^2) \\ p_0 &= a_0 \tau_0 \sqrt{\frac{2}{E}} \left[\left(\frac{2}{A+E} - c_0 \right) \frac{1}{\sqrt{D}} \operatorname{tg}^{-1} G(\theta) + \left(\frac{1}{A+E} + c_0 \frac{C}{2} \right) \right. \\ &\quad \left. \cdot \frac{1}{\sqrt{CD}} \ln \frac{\sqrt{C} + H(\theta)}{\sqrt{C} - H(\theta)} \right] \quad (12)\end{aligned}$$

其中

$$G(\theta) = \frac{\sqrt{2(E+A)} \kappa_0 \sin \theta}{E + A - 2(1 - \kappa_0 \cos \theta)} \quad H(\theta) = \frac{E - A + 2(1 - \kappa_0 \cos \theta)}{\sqrt{2(E+A)} \kappa_0 \sin \theta} \quad (13)$$

A, B, C, D, E 分别为下列常数

$$\begin{aligned}A &= 1 - \kappa_0^2 - \tau_0^2, \quad B = 2\tau_0, \quad C = \frac{E-A}{E+A} \\ D &= \frac{4E}{E+A}, \quad E = \sqrt{A^2 + B^2}\end{aligned} \quad (14)$$

积分常数 c_0 可利用周期性条件(11)式定出

$$c_0 = \frac{1}{\tau_0} \operatorname{tg} \frac{\beta}{2} \quad \left(\beta = \operatorname{tg}^{-1} \frac{B}{A} \right)$$

由(4)式中 p 的级数展开式, 可以写出无量纲压力梯度在轴线方向的分量为

$$\frac{\partial \bar{p}}{\partial z} = a_0 + \varepsilon a_1 + \varepsilon^2 a_2 + \cdots$$

其中 $a_0, a_1, a_2, \cdots$ 是待定常数。可利用无量纲流量表达式(6), 推导出确定这些常数的条件。由于无量纲流量

$$Q = \frac{1}{U\pi R^2} \int_0^{2\pi} d\theta \int_R^{R+a} v^n r dr$$

$$\begin{aligned}
& - \frac{1}{U\pi R^2} \int_0^{2\pi} d\theta \int_0^1 \varepsilon U(v_0^n + \varepsilon v_1^n + \varepsilon v_2^n + \cdots) R^2 (1 + \varepsilon \eta) d\eta \\
& - \frac{\varepsilon}{\pi} \int_0^{2\pi} d\theta \int_0^1 [v_0^n + \varepsilon(\eta v_0^n + v_1^n) + \varepsilon^2(\eta v_1^n + v_2^n) + \cdots] d\eta
\end{aligned}$$

与(6)式进行量阶比较,可得

$$\frac{1}{\pi} \int_0^{2\pi} d\theta \int_0^1 v_0^n d\eta = 2 \quad (15.1)$$

$$\frac{1}{\pi} \int_0^{2\pi} d\theta \int_0^1 (\eta v_0^n + v_1^n) d\eta = 1 \quad (15.2)$$

$$\frac{1}{\pi} \int_0^{2\pi} d\theta \int_0^1 (\eta v_i^n + v_{i+1}^n) d\eta = 0 \quad (i = 1, 2, 3, \cdots) \quad (15.3)$$

利用上述各式, 不难确定 $a_i (i = 0, 1, 2, \cdots)$. 现在只要将(12)式中的 v_0^n 表达式代入(15.1)式中, 即可求出

$$a_0 = \frac{-12\sqrt{E}}{\cos \frac{\beta}{2} + c_0 \tau_0 \sin \frac{\beta}{2}}$$

3. 一阶摄动解

关于 ε 的一阶方程组如下:

$$\begin{aligned}
\frac{\partial v_1'}{\partial \eta} + \frac{\partial v_1^\theta}{\partial \theta} - \frac{\tau_0}{m_0} \frac{\partial v_1^n}{\partial \theta} + \frac{m_0'}{m_0} v_1^\theta &= \frac{\tau_0(1-m_0)\eta}{m_0'} \frac{\partial v_0^n}{\partial \theta} + \eta \frac{\partial v_0^\theta}{\partial \theta} \\
&\quad - \frac{(1-m_0)m_0\eta}{m_0} v_0^\theta - \left(2 - \frac{1}{m_0}\right) v_0^n \\
\frac{\partial p_1}{\partial \eta} &= 0 \\
\frac{\partial p_1}{\partial \theta} - \frac{\partial^2 v_1^\theta}{\partial \eta^2} &= \eta \frac{\partial p_0}{\partial \theta} + \left(2 - \frac{1}{m_0}\right) \frac{\partial v_0^\theta}{\partial \eta} \\
\frac{1}{m_0} \left(a_1 - \tau_0 \frac{\partial p_1}{\partial \theta}\right) - \frac{\partial^2 v_0^n}{\partial \eta^2} &= \frac{m_0 - 1}{m_0'} \eta \left(a_0 - \tau_0 \frac{\partial p}{\partial \theta}\right) + \left(2 - \frac{1}{m_0}\right) \frac{\partial v_0^n}{\partial \eta} \quad (16)
\end{aligned}$$

边界条件与零阶方程类似, 在 $\eta = 0, \eta = 1$ 的壁面上, $v_1' = v_1^n = v_1^\theta = 0$; 另外 $p_1, v_1', v_1^\theta, v_1^n$ 满足周期性条件.

经过复杂的积分运算, 可得一阶摄动解

$$\begin{aligned}
v_1' &= \frac{a_0 \tau_0 m_0'}{12 m_0 (m_0^2 + \tau_0^2)^2} \left(c_0 m_0' - 4 m_0 - 4 c_0 \tau_0' - \frac{c_0 \tau_0^2}{m_0} \right) (\eta^4 - 2 \eta^3 + \eta^2) \\
v_1^\theta &= -\frac{a_1}{2} \frac{\tau_0 (1 - c_0 m_0)}{m_0^2 + \tau_0^2} (\eta - \eta^2) + \frac{a_0 \tau_0}{12 m_0 (m_0^2 + \tau_0^2)} \left\{ (1 - c_0 m_0) \right. \\
&\quad \cdot [(2 - 6 m_0) \eta^3 + (6 m_0 - 3) \eta^2 + \eta] + 3 m_0 (c_0 - c_1 m_0 \\
&\quad \left. + 2 m_0 \frac{1 - c_0 m_0}{m_0' + \tau_0^2}) (\eta^2 - \eta) \right\} \\
v_1^n &= -\frac{c_1}{2} \frac{m_0 + c_0 \tau_0^2}{m_0' + \tau_0^2} (\eta - \eta^2) + \frac{a_0}{12 m_0 (m_0^2 + \tau_0^2)} \left\{ (m_0 + c_0 \tau_0^2) \right.
\end{aligned}$$

$$\begin{aligned}
& \cdot [(4 - 6m_0)\eta^3 + (6m_0 - 3)\eta^2 - \eta] - 3\tau_0^2 \left(c_0 - c_1 m_0 \right. \\
& \left. + 2m_0 \frac{1 - c_0 m_0}{m_0^2 + \tau_0^2} \right) (\eta^2 - \eta) \Big\} \\
p_1 = & a_1 \tau_0 \sqrt{\frac{2}{E}} \left[\left(\frac{2}{A + E} - c_0 \right) \frac{1}{\sqrt{D}} \operatorname{tg}^{-1} G(\theta) + \left(\frac{1}{A + E} + c_0 \frac{C}{2} \right) \right. \\
& \left. \cdot \frac{1}{\sqrt{CD}} \ln \frac{\sqrt{C} + H(\theta)}{\sqrt{C} - H(\theta)} \right] + \frac{a_0 \tau_0}{2} [c_0 J_1(\theta) - c_1 J_2(\theta) + 2J_3(\theta) - 2c_0 J_4(\theta)]
\end{aligned} \quad (17)$$

其中积分 $J_i(\theta)$ 的表达式如下

$$\begin{aligned}
J_1(\theta) &= \int_0^\theta \frac{d\theta}{m_0^2 + \tau_0^2} = \frac{2\sqrt{2E}}{E(A + E)} [I_1(\theta) + I_2(\theta)] \\
J_2(\theta) &= \int_0^\theta \frac{m_0 d\theta}{m_0^2 + \tau_0^2} = [I_2(\theta) - CI_1(\theta)] \\
J_3(\theta) &= \int_0^\theta \frac{m_0 d\theta}{(m_0^2 + \tau_0^2)^2} = \frac{2\sqrt{2E}}{E^2(A + E)} [(2 - C)I_1(\theta) + I_2(\theta) \\
&\quad + C(C - 3)I_3(\theta) + (1 - 3C)I_4(\theta)] \\
J_4(\theta) &= \int_0^\theta \frac{m_0^3 d\theta}{(m_0^2 + \tau_0^2)^2} = J_1(\theta) - \frac{B^2 \sqrt{2E}}{E^2(A + E)^2} [3I_1(\theta) + I_2(\theta) \\
&\quad + (1 - 3C)I_3(\theta) + (3 - C)I_4(\theta)]
\end{aligned}$$

上式中 $I_i(\theta)$ 的表达式为

$$\begin{aligned}
I_1(\theta) &= \frac{1}{2\sqrt{CD}} \ln \frac{\sqrt{C} + H(\theta)}{\sqrt{C} - H(\theta)} \\
I_2(\theta) &= \frac{1}{\sqrt{D}} \operatorname{tg}^{-1} G(\theta) \\
I_3(\theta) &= \frac{1}{2CD} (CF + D)I_1(\theta) - \frac{(F + 2E)H(\theta)}{\sqrt{D}[H^2(\theta) - C]} \\
I_4(\theta) &= \frac{F}{2D} \left[\frac{G(\theta)}{\sqrt{D}[G^2(\theta) + 1]} + I_2(\theta) \right]
\end{aligned}$$

上述式中 $A, B, C, D, E, G(\theta), H(\theta)$ 的表达式如(13), (14)式所示; 常数 $F = 2 - A - E$. 积分常数 c_1 可利用周期性条件定出

$$c_1 = \frac{1}{E\tau_0 \cos \frac{\beta}{2}} \left[(1 - c_0 \tau_0^2) \sin \frac{3\beta}{2} - \tau_0(1 + c_0) \cos \frac{3\beta}{2} \right]$$

常数 a_1 可通过(15-2)式定出

$$a_1 = \frac{1}{2E \left(\cos \frac{\beta}{2} + c_0 \tau_0 \sin \frac{\beta}{2} \right)} \left\{ \left[-c_1 E \tau_0 \sin \frac{\beta}{2} + (c_0 \tau_0^2 - 1) \cos \frac{3\beta}{2} \right] \right.$$

$$-(1 + \epsilon_0)\tau_0 \sin \frac{3\beta}{2} \left\{ a_0 - 12E\sqrt{E} \right\}$$

从上述零阶与一阶摄动解已经可以看出, 环形截面上存在二次流动。

四、圆弧管道中环形截面上的二次流

螺旋管道中心轴线的挠率 $\tau = 0$ 时, 即成为圆弧管道。此时的零阶, 一阶摄动解只需令(12)式, (17)式中的 $\tau_0 \rightarrow 0$, 即可获得零阶摄动解

$$\begin{aligned} v_0' &= v_0'' = 0, \quad p_0 = 0 \\ v_0^* &= -\frac{a_0}{2} \frac{1}{m_0} (\eta - \eta^2), \quad a_0 = -12\sqrt{1 - \kappa_0^2} \end{aligned} \quad (18)$$

一阶摄动解为

$$\begin{aligned} v_1' &= v_1'' = 0, \quad p_1 = 0 \\ v_1^* &= -\frac{a_1}{2} \frac{1}{m_0} (\eta - \eta^2) + \frac{a_0}{12m_0^2} [(4 - 6m_0)\eta^3 + (6m_0 - 3)\eta^2 - \eta] \\ a_1 &= 6\kappa_0^2/\sqrt{1 - \kappa_0^2} \end{aligned} \quad (19)$$

不难看出, 此时 $v_i' = v_i'' = 0, (i = 0, 1)$, 截面上还未出现二次流, 为此需进一步求解 ϵ 的二阶方程:

$$\begin{aligned} \frac{\partial v_2}{\partial \eta} + \frac{\partial v_2^*}{\partial \theta} + \frac{m_0}{m_0'} v_2^* &= \left[\eta \frac{\partial v_1''}{\partial \theta} - \frac{(1 - m_0)m_0'}{m_0^2} \eta v_1'' - \frac{2m_0 - 1}{m_0} v_1' \right] \\ &\quad - \left[\eta^2 \frac{\partial v_0^*}{\partial \theta} + \frac{(1 - m_0)^2 m_0}{m_0^3} \eta^2 v_0'' - \frac{m_0' + (1 - m_0)^2}{m_0^3} \eta v_0' \right] \\ \frac{\partial p_2}{\partial \eta} &= \frac{\partial^2 v_0}{\partial \eta^2} \\ \frac{\partial p_2}{\partial \theta} - \frac{\partial^2 v_1^*}{\partial \eta^2} &= \left(\eta \frac{\partial p_1}{\partial \theta} - \frac{2m_0 - 1}{m_0} \frac{\partial v_1''}{\partial \eta} \right) - \text{Re} \left[v_0' \frac{\partial v_0^*}{\partial \eta} - v_0^* \frac{\partial v_0'}{\partial \theta} - \frac{m_0'}{m_0} (v_0^*)^2 \right] \\ &\quad + \frac{\partial^2 v_0^*}{\partial \theta^2} - \frac{m_0' + (1 - m_0)^2}{m_0^3} \eta \frac{\partial v_0^*}{\partial \eta} + \frac{m_0'}{m_0} \frac{\partial v_0^*}{\partial \theta} - \frac{m_0 + m_0'^2}{m_0^2} v_0^* - \eta^2 \frac{\partial p}{\partial \theta} \\ \frac{\partial^2 v_2^*}{\partial \eta^2} &= \frac{a_2}{m_0} - \left(\frac{m_0 - 1}{m_0'} \eta + \frac{2m_0 - 1}{m_0} \frac{\partial v_1''}{\partial \eta} \right) + \text{Re} \left[v_0' \frac{\partial v_0^*}{\partial \eta} + v_0^* \frac{\partial v_0'}{\partial \theta} + \frac{m_0'}{m_0} v_0' v_0^* \right] \\ &\quad - \left[\frac{\partial^2 v_0^*}{\partial \theta^2} - \frac{m_0' + (1 - m_0)^2}{m_0^3} \eta \frac{\partial v_0^*}{\partial \eta} + \frac{m_0}{m_0} \frac{\partial v_0^*}{\partial \theta} - \frac{\kappa_0^2}{m_0^2} v_0^* - \frac{a_0(1 - m_0)^2}{m_0^3} \eta^2 \right] \end{aligned} \quad (20)$$

将零阶解(18)式, 一阶解(19)式代入上述方程, 积分后可获得

$$\begin{aligned} v_2' &= \frac{a_0' \text{Re } m_0 m_0' - 2m_0}{1680 m_0'} (2\eta^6 - 7\eta^5 + 7\eta^3 - 3\eta^2 + \eta^2) \\ v_2^* &= \frac{a_0' \text{Re } m_0'}{1680 m_0^3} (-14\eta^6 + 42\eta^5 - 35\eta^4 + 9\eta^2 - 2\eta) \\ v_2'' &= \frac{a_2}{2m_0} (\eta^2 - \eta) + \frac{a_1}{12m_0^2} [(4 - 6m_0)\eta^3 + (6m_0 - 3)\eta^2 - \eta] \end{aligned}$$

$$\begin{aligned}
 & + \frac{a_0}{24m_0^3} [(8m_0^2 - 8m_0 + 3 + 4\kappa_0^2)\eta^4 - (4m_0^2 + 2m_0 - 2 + 8\kappa_0^2)\eta^3 \\
 & + (2m_0 - 1)\eta^2 - (4m_0^2 - 8m_0 + 4 - 4\kappa_0^2)\eta] \\
 p_2 = & -\frac{3}{560} a_0^2 \text{Re} \left[\frac{1}{m_0^2} - \frac{1}{(1 - \kappa_0^2)^2} \right] \quad (21)
 \end{aligned}$$

将 v_2^* 表达式代入(15-3)式,积分后可计算出

$$\begin{aligned}
 a_2 = a_0 \left[\frac{3}{10} \sqrt{1 - \kappa_0^2} + \frac{77}{60(1 - \kappa_0^2)} - \frac{37}{60(1 - \kappa_0^2)^2} + \frac{11\kappa_0^2}{120(1 - \kappa_0^2)^2} \right. \\
 \left. + \frac{\kappa_0^4}{5(1 - \kappa_0^2)^2} - \frac{59}{60} \right] - a_1 \frac{1}{2(1 - \kappa_0^2)} \quad (22)
 \end{aligned}$$

由上述二阶解可以看出,此时在截面上出现二次流,二次流的流线方程应满足

$$\frac{1}{r} \frac{dr}{d\theta} = \frac{v'}{v^\theta} = \frac{\varepsilon v_2'}{v_2^\theta} = \varepsilon \frac{m_0 m_0'' - 2m_0'^2}{m_0 m_0'} \frac{2\eta^7 - 7\eta^6 + 7\eta^5 - 3\eta^3 + \eta^2}{-14\eta^6 + 42\eta^5 - 35\eta^4 + 9\eta^2 - 2\eta}$$

注意到 $r = (1 + \varepsilon\eta)R$, $m_0 = 1 - \kappa_0 \cos \theta$,积分上式可得

$$\frac{\eta^2(1 - \eta)^a (|1 - 2\eta|)^b (-2\eta + 1 - \sqrt{5})^c (2\eta - 1 + \sqrt{5})^d \sin \theta}{(1 + \varepsilon\eta)^e (1 - \kappa_0 \cos \theta)^2} = \phi \quad (23)$$

其中

$$\begin{aligned}
 a = \frac{2}{1 + \varepsilon}, \quad b = \frac{2}{2 + \varepsilon}, \quad c = \frac{2}{2 + \varepsilon(1 + \sqrt{5})}, \quad d = \frac{2}{2 + \varepsilon(1 - \sqrt{5})} \\
 e = \frac{14 + 28\varepsilon + 7\varepsilon^2 - 7\varepsilon^3 - 2\varepsilon^4}{2 + 5\varepsilon + 2\varepsilon^2 - 2\varepsilon^3 - \varepsilon^4}
 \end{aligned}$$

ϕ 是流线族的积分常数,给定一个 ϕ ,对应一条流线。上述式中 $m_0'' = \frac{d^2 m_0}{d\theta^2} = x_0 \cos \theta$ 。

五、结果讨论

环形截面的直线管道中的粘性流动有精确解。按照前述的无量纲化,且假定 $\frac{dp}{dz} = a_*$, 精确解为

$$\begin{aligned}
 v_*' = v_*^\theta = 0 \quad p_* = a_* z \\
 v_*^r = \frac{a_*}{2} \left[\left(\frac{1}{2} \eta^2 + \frac{1}{\varepsilon} \eta \right) - \left(\frac{1}{2} + \frac{1}{\varepsilon} \right) \frac{\ln(1 + \varepsilon\eta)}{\ln(1 + \varepsilon)} \right]
 \end{aligned}$$

为便于比较,上述解可表示成 ε 的幂级数

$$\begin{aligned}
 p_* = [a_0^* + \varepsilon a_1^* + \varepsilon^2 a_2^* + o(\varepsilon^3)] z \\
 v_*^r = \frac{a_0^*}{2} (\eta^2 - \eta) + \varepsilon \left[\frac{a_1^*}{2} (\eta^2 - \eta) + \frac{a_0^*}{12} (-2\eta^3 + 3\eta^2 - \eta) \right] \\
 + \varepsilon^2 \left[\frac{a_2^*}{2} (\eta^2 - \eta) + \frac{a_1^*}{12} (-2\eta^3 + 3\eta^2 - \eta) + \frac{a_0^*}{24} (3\eta^4 - 4\eta^3 + \eta^2) \right] + o(\varepsilon^3)
 \end{aligned}$$

其中 a_0^*, a_1^*, a_2^* 可按(15)式给出的原则确定为

$$a_0^* = -12, \quad a_1^* = 0, \quad a_2^* = \frac{1}{5}$$

在前面求解获得的螺旋管和圆弧管的各阶摄动解中,当 $\kappa_0 = 0, \tau_0 \rightarrow 0$ 时,结果和直管精确解完全一致。

从已经获得的摄动解,可看出以下几点结论:

(1) 螺旋管道环形截面上存在二次流。由零阶解 $v_0^\theta = 0$, 只出现 v_2^θ 可以看出二次流表现为沿圆周方向的流动。图 3 给出了 $\eta = \frac{1}{6}$ 处, v_2^θ 沿 θ 的变化曲线,对照图 6 压力变化曲线可以发现,二次流由截面上压力极大值点沿圆周正反两个方向流向压力极小值点。

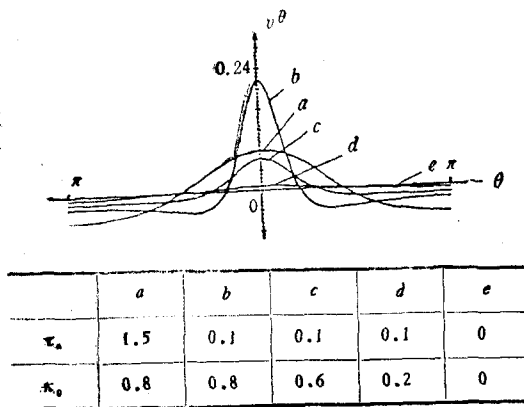


图 3 环形截面上 v_2^θ 沿周向的变化曲线

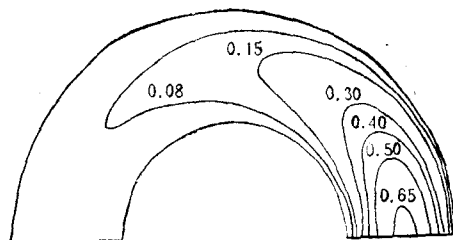


图 4 环形截面上 v_2^r 的等速度线

(2) 螺旋管道环形截面上法向速度 v^r 沿周向分布不均匀。由图 4 给出环形截面上 v^r 的等速度线,可以看出: 相同半径处,靠近螺旋管内侧的 v^r 要比外侧大。图 5 是 v^r 沿径向的平均速度

$$\bar{v}^r = \bar{v}^r(\theta) = \int_0^1 (v_0^r + \varepsilon v_1^r) d\eta$$

在不同 κ_0, τ_0 值时的曲线 ($\varepsilon = 0.1$)。可以明显看出,通过螺旋管道的流量,相对集中于管道内侧 ($\theta = 0$)。曲率 κ_0 越大,这种倾向越显著。

(3) 螺旋管道环形截面上的压力沿周向分布是不均匀的。图 6 是截面上的相对压力 $p' = p'(\theta) = p_0(\theta) + \varepsilon p_1(\theta)$ 在不同 κ_0, τ_0 值时的曲线。它显示压力在截面上存在一个

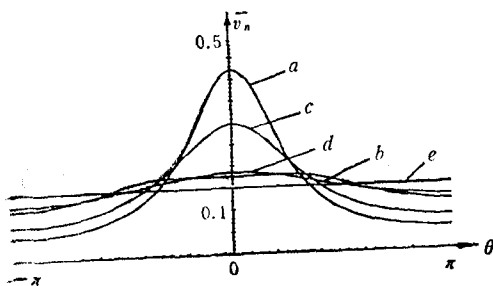


图 5 环形截面上 $\bar{v}^r$ 沿周向的变化曲线

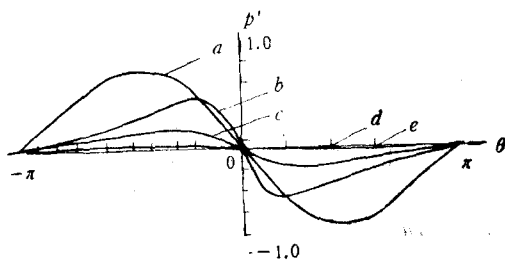


图 6 环形截面上压力沿周向变化曲线

极大值点和一个极小值点, 它们处于相对内弯点($\theta = 0$)对称的上下位置上。当 τ_0 一定时, 随着曲率 κ_0 的增加, 极值点向内弯点靠近。正是由于存在这种沿周向不均匀的压力分布, 形成了截面的周向的二次流。

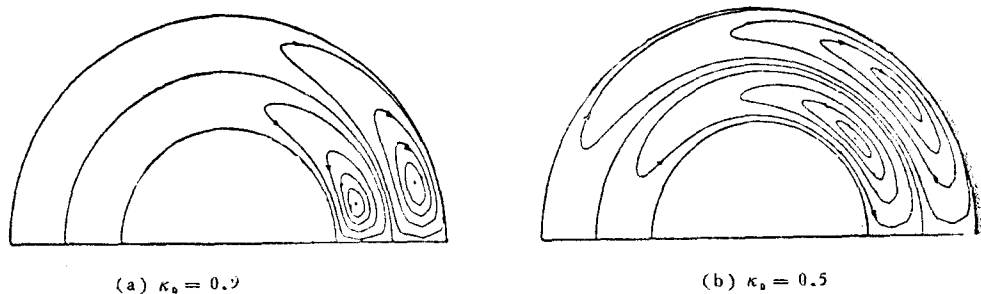


图7 圆弧管道环形截面上的二次环流涡

(4) 圆弧管道环形截面上的二次流是上下对称分布的四个环流涡。当曲率 κ_0 增大时, 环流涡的中心点向内弯点方向移动。图7是根据流线方程(23)式给出的二次流的环流涡。由 ε 的二阶方程不难看出, 圆弧管道环形截面上二次流的出现是由于惯性力影响的结果。

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VISCOUS FLOW IN HELICAL PIPES WITH NARROW ANNULAR CROSS SECTION

Zhang Benzhuo

(Zhejiang University, 310027, China)

D. N. Fan

(Howard University, DC. 20059, U. S. A)

Abstract The Navier-Stokes equations are established for a nonorthogonal coordinate system based on tensor analysis. The zeroth-, the first- and the second-order ($\tau=0$) analytic solutions are obtained for fully developed flow in helical pipes with narrow annular cross section using a perturbation method. It is found that there is a secondary flow on the annular cross section.

Key words tensor application, flow in helical pipes, secondary flow, perturbation solution